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NAVAL RESEARCH LABORATORY
Washington, D. C.

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Chemistry Division - Physical & Inorganic Section

30 September 1946

QUARTERLY PROGRESS REPORT ON THE MEASUREMENT OF THE PHYSICAL AND CHEMICAL PROPERTIES OF THE SODIUM-POTASSIUM ALLOY. No. 1

by
C. T. Ewing, R. R. Miller

- Report P-3010 -

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NRL Problem P-149

ABSTRACT

T he alloys of Potassium-Sodium are under study as a heat transfer medium. Physical and chemical properties, along with measurements of heat transfer coefficients on an engineering scale, are being studied. This report is concerned more with the description of apparatus and methods than with measured results; however, preliminary measurements on density and viscosity are included.

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D. Report on "Determination of the Thermal Conductivity of Sodium-Potassium Alloy at Elevated Temperatures"-Deem and Russell.

E. National Defense Research Committee Division B, Section L-6. Report on "Vapor-Liquid Equilibria for Mixtures of Alkali Metals", NRL 2958.

F. Preliminary Report #2 - Theory of "Figure of Eight" Heat Exchanger by W. L. McCabe and R. A. Tidball.

INTRODUCTION

Authorization

The study on the physical and chemical properties of Potassium Sodium Alloy was authorized by BuShips Project 990/46.

Statement of Problem

1. The program of study presented and discussed with personnel of the Bureau has been followed with respect to the phases of problem being investigated by the Laboratory and contracted to the Mine Safety Appliance Company See App. A). This report combines the results obtained by the two groups along with other data pertinent to the program.

2. The Laboratory has designed and constructed apparatus to measure some of the physical properties of alloys of potassium and sodium. The properties to be measured immediately were viscosity, thermal conductivity, specific heat, and the determination of the liquid solid phase diagram. Other properties such as densities, heat transfer coefficients and a study of the handling of the alloy are being conducted under a Laboratory contract with the Mine Safety Appliances Company of Pittsburgh, Pa. Other properties and characteristics which appear to deserve study will be determined to the extent justified by the project. Certain of the unseen difficulties are being solved. They are problems inherent in purification, transferring and maintaining the alloy in suitably pure condition. The careful purification of blanketing gases and transferring them in glass free from rubber tubing has been necessary to maintain purity of the alloys. The purification of the metals and alloys has been satisfactory for the desired measurements only when the alloys were freshly distilled or stored with extreme care. Distillations so far have been made in glass; however, a distillation unit of metal is nearing completion.

3. While results of work on the program is not as far advanced as was anticipated for this date, the status of the active measurements are reported in the following paragraphs.

PHYSICAL PROPERTY MEASUREMENTS

Alloy Samples

4. Seven (7) samples of alloy have been chosen as standards for the measurement of all physical properties and 200 pounds of each has been made up by and stored at the Mine Safety Appliances Company plant. The samples were chosen with respect to the published phase diagram such that freezing points of the samples would essentially define the phase diagram itself. The composition of the samples is given below with their corresponding numbers.

Sample	Wt. % K	Wt. % Na
1	100	0
2	93	7
3	80	20
4	66	34
5	44	56
6	33	67
7	0	100

Viscosity

5. Preliminary measurements on viscosity were reported in NRL Report P-2931, 14 August 1946 (App. B). The measurements reported were for 43.3% potassium from 65.5°C to 600°C. The viscosity in centipoises was 0.514 at 65.5° falling with temperatures at a decreasing rate to 0.256 at 600° with a slight rise indicated between 600 and 700°C. These values were reported with a probable error of ± 10%. The accuracy cannot be claimed as being any better at this date, but the indicated rise in the viscosity above 600°C has not been substantiated.

6. The metal apparatus in use was described in the above report. Measurement of viscosity of the 65% potassium alloy is underway. In addition to the apparatus, a quartz Ostwald viscometer has been constructed and is ready for calibration. The distillation in glass indicates that pure alloy will present a suitable meniscus in a transparent viscometer. It will be usuable on a few hundred degrees, if not over the full range.

Density

7. The density of the alloys were measured by MSA by the method of weighing a plumb-bob in the liquid alloys. This method was previously used by Rinck for the determination of density at elevated temperatures on sodium and potassium. The densities were measured over a range from room temperature to 700°C with constant and what appeared to be satisfactory values obtained only at the higher temperature range. From 350 to 450°C, a point, depending on the composition, developed below which reproducible values could not be obtained with the plumb-bob method. For lower temperatures, a dilatometer was used which gave reproducible values. However, in some cases the density against temperature curves for the two methods do not have exactly the same slope. For the 50-50 mixture, the density varied from 0.876 gm/cc at 100°C to 0.738 gm/cc at 700°C, while sodium varied from approximately 0.94 to approximately 0.775 of the same temperature range. The density of potassium over the same temperature range varied from approximately 0.82 to 0.67. The report on density from MSA is enclosed as App. C.

Specific Heat

8. A metal Dewar flask apparatus has been constructed of mild iron and stainless steel. The containing flask is of mild iron with a nickel plate on the exterior and neck of thin

stainless steel tube. The inside container is threaded into the housing flask which has a nickel plated interior. The vacuum space is maintained at low pressure by continual pumping. The heater, stirrer and thermocouple are placed in the flask through thin stainless tubes which are closely baffled through the neck section to reduce convection from the metal surface.

9. Preliminary measurements have indicated that the specific heat of the alloy can be calculated directly from the specific heat of the elements and the concentrations. The specific heat against temperature curves appears to follow a gradually falling curve for the 43.3% K alloy indicating no sharp change in the molecular state of the alloy.

10. This unit has shown satisfactory results on preliminary operation and should furnish data on specific heat in a relatively short time.

Thermal Conductivity

11. An apparatus has been designed and constructed which in plan is similar to that used by Professor Bidwell of Lehigh University, for the study of heat conduction in molten metals. It is essentially a vertical cylinderical container with a heater at the top of the sample and a heat well at the bottom. The whole unit is raised to a constant temperature and then with added heat in the top heater, an equilibrium is established, and from the measure of the gradients in the sample and insulation, the heat conductivity of the sample can be calculated. This method appears to be more satisfactory for the alloys than others which have been reviewed and discussed, and is the opinion of Professor Bidwell that the apparatus will give the desired accuracy on measurements. Measurements will be made in the second quarter. It is planned to have Professor Bidwell employed as a consultant on this phase of the problem. Measurements were made on thermal conductivity of 51.7% sodium, 48.3% potassium alloy for the Argonne Laboratory by the Battelle Memorial Institute. Measured results given in watts cm^{-2} cm $°C^{-1}$ were 0.258 at 100°C to 0.284 at 500°C. Copy of the report is enclosed as App. D.

Liquid-Solid Phase Diagram

12. An impressive amount of work has been done on this phase diagram and the later values appear to be in good accord. Thus it may be necessary only to check a few compositions of well purified metals in order to arrive at a satisfactory conclusion concerning the solid-liquid diagram. Apparatus has been set-up in which the freezing point of the liquid will be determined. In all probability this phase of the problem can be satisfactorily cleared up in a period of a month or two.

Vapor-Liquid Phase

13. During the work at this laboratory on the distillation of potassium for the production of oxide, the vapor liquid equi-

librium for the alloys was of interest. The problem was suggested to NDRC at the time, and Dr. G. B. Kistiakowsky as Chief Investigator studied the vapor liquid phase and published a report of the measured values. A copy of this report is enclosed as App. E.

Temperatures at which KNa alloys "wet" metals.

14. A nickel crucible which could be maintained at elevated temperatures by an integral heater was enclosed in a glass flask where the atmosphere could be controlled. Samples of metals could be raised and lowered into the alloy in the crucible by means of a glass shaft which rotated through a ground glass joint and extended over the crucible. Samples were connected to the shaft by thin wire which was wound on or off the shaft as the sample was raised or lowered. The meniscus between the alloy and the metal was observed during the lowering of the sample to determine at what temperature the metal surface was "wet" by the alloy. A depressed meniscus was recorded as not "wetting" while a flat or raised meniscus at the metal was recorded as "wetting". The strip metal samples were allowed to submerge in the KNa alloy between dipping tests to maintain them at the temperature of the liquid alloy. The results recorded for metals and alloys are given below.

Summary of all conclusions on "wetting" tests

Metal	30%K(by wt)	45%K	65%K
Soft Iron	270°C	(a) 275°C (b) 330° 295°	(c) 310°C
Stainless Steel	260°	(a) 260° (b) 370° 290	(c) 320°
Nichrome	(b)340° 320°	(a) 270° (a) 275° 330°	340°
Nickel	(b)350° 345°	(a) 320° 320°	350°

(a) These tests were the first ones run, when mineral oil was used and possibly contaminated the metal sample.

(b) It was believed that the thermocouple was slightly in error during these tests.

(c) These two temperatures were not actually reached; but were approached closely enough to give a satisfactory prediction.

Heat Transfer Coefficient

15. A fluid film on a solid is the greatest cause of resistance to heat flow from a moving fluid to the solid. A measurement of the resistance of heat flow in a system can be made by a complete measurement of the temperatures in a vicinity of heat transfer boundaries or it may be determined indirectly by calculations. The equation for the calculations has been derived by MSA and is given in App. F. The resistance to heat flow of an individual film is dependent on two dimensionless groups; the Reynolds Number and the Prandtl Number. The effects of the Reynolds Number are well known, but the effects are unknown for very low Prandtl Numbers. The Prandtl numbers for NaK alloy are much lower than those for fluids normally used for heat transfer medium. The method described in App. F. is designed to isolate the Prandtl number factor.

CONCLUSION

A study on the measurements of the properties is being continued.

Program on the Study of Sodium Potassium Alloy
25 June 1946

This program is planned to be carried out by Naval Research Laboratory with some of the engineering features and measurements subcontracted to Mine Safety Appliance Company at Pittsburgh, Pa.

Physical Properties

A. Solid-liquid phase diagram. - NRL: Apparatus is being assembled to determine freezing points on the alloys on hand and compositions to be made here. This appears necessary to check on the composition of samples since freezing points can be readily taken. - MSA: May also collect some data.

B. Liquid-Vapor phase diagram (no work planned immediately)

C. Specific Heat apparatus being constructed. No MSA work planned.

D. Viscosity - NRL: Apparatus for measurements in the planning stage.

E. Thermal Conductivity - NRL: Drawing of an apparatus is under way. The liquid thermal conductance apparatus in common use must be redesigned for alloy.

F. Density - MSA: MSA is making density measurements on the density of the alloys by the method of Rinck-i.e., weighing a metal plumb-bob in the alloy over a range of temperatures.

NRL has planned to make some measurements on density in glass over the lower part of the temperature range. MSA has requested one or two of the glass bulbs we planned on using. They will no doubt make measurements in them over a similar range.

G. Surface Tension - NRL: No immediate plans.

H. Electrical Conductivity - NRL: Empericals relation have been presented between the electrical and thermal conductivity. They will be examined and measurements made at this time, only if they appear to be of value in perfecting heat conductivity data.

I. Magnetic Susceptibility - NRL or MSA (No work planned immediately)

Chemical Properties

A. General Reactions

(1) With H_2O NRL: Now under way; MSA: In small heat

APPENDIX A

interchanger type models.

(2) Reaction with halogenated compounds and organics (gasket materials) NRL MSA

Deoxidation and decarbonization of metals and alloys. NRL and MSA and Chicago. - Methods not yet planned at NRL or MSA.

Argonne Laboratory at Chicago has some data showing carbon is removed from steel by alloys, and that stainless steel shows corrosion probably due to the oxygen layer.

Organic reaction with alloy NRL with no definite plans at present. Would be of interest on problem of gaskets for system if necessary.

Methods of Handling, Storing, Shipping and Transfering.- MSA. NRL will furnish what data is available from the work here.

Contaminants of Potassium Sodium Alloy -- Oxides Nitrides, Sulfides, carbides, hydrides, carlonyl, hydroxides.

NRL plans are for this work to be delayed to a little later date or contracted out to a University.

Experimental heat transfer unit - MSA,

A. Construction
B. Operation to verify research information (1), (2), (3) and (4):

(1) Determine heat transfer coefficients

(a) Stationary
(b) Low Reynolds numbers
(c) High Reynolds numbers

(2) Tube bundle
(3) Pumps
(4) Valves and fittings
(5) Life at 1200°F and at 1500°F

Corrosion and Erosion:

A. Corrosion
B. Erosion
C. Methods to minimize (A) and (B)

Continue on work in Chicago

APPENDIX A

Navy Department - Office of Research and Inventions

NAVAL RESEARCH LABORATORY
Washington, D.C.

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CHEMISTRY DIVISION - PHYSICAL AND INORGANIC SECTION

14 August 1946

PRELIMINARY REPORT ON VISCOSITY DETERMINATIONS ON A POTASSIUM-SODIUM ALLOY

By R. Ruskin, C.T. Ewing, and
R.R. Miller

- Report P-2931 -

* * *

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ABSTRACT

An Ostwald type viscometer has been used to measure values of viscosity on a potassium-sodium alloy which was 43.4% potassium by weight. Viscosity of the alloy at 72°C was 1.267 relative to water at the same temperature. The values at higher temperatures were calculated from the volumes of alloy flowing per second at those temperatures, and the constant determined for the apparatus at 72°C.

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INTRODUCTION

A. Authorization

1. This project was authorized by BuShips Project Order No. 990/46 dated June 24, 1946.

B. Statement of Problem

2. The project covers the library and laboratory research necessary to arrive at satisfactory values for the physical properties of Sodium and Potassium alloys. The viscosity has been determined, on an alloy, for 43.4% K by weight. These values are the basis of this preliminary report.

C. Known Facts Bearing on the Problem

3. Absolute viscosities may be calculated from measurements made in a number of different types of apparatus. The type of apparatus to be used is determined to a great extent by the characteristics of the liquids under study. For the alloys which are particularly reactive with moisture and oxygen, completely closed viscometers are necessary. A preferred method of getting absolute viscosity; that is the falling-ball method with calculations based on Stoke's Law would be somewhat difficult at the high temperatures in an opaque viscometer. The more readily used method is a variation of the Ostwalt viscometer where the amount of alloy flowing in the capillary tube can be determined against time. At the same temperatures and under the same pressure head, measurements made on two fluids will give a viscosity measurement of one relative to the other. Water is customarily used as a reference fluid and then from the absolute viscosity of water, the absolute viscosity of the alloy at the same temperature can be calculated. This is the procedure which has been followed in the measurements tabulated at the end of the report. The relative viscosity has been calculated from the relation

$$\frac{n_1}{n_2} = \frac{d_1 t_1}{d_2 t_2}$$

where n_1 and n_2 are the viscosities of alloy and water respectively, d_1 and d_2 the densities, t_1 and t_2 the time required for equal volume of the fluids to flow. From the relative viscosity multiplied by the absolute viscosity of water at the same temperature, the absolute viscosity of the metals is determined at that temperature. This value of the viscosity with the relation $n = \frac{k}{v}$ gives a value for the constant k for the apparatus. n was the viscosity of the alloy and v the volume of alloy flowing in unit time. In this preliminary study the value of k was considered constant for the temperature range. This constant, with the volumes determined at temperature intervals, was

used to calculate the absolute viscosity over the temperature range given.

METHODS

A. Apparatus

4. An apparatus consisting of two horizontal tanks connected by a small capillary tube was constructed so that an upper tank (#1 on plate 1) and the coil of the capillary tube were enclosed in an electrically-heated furnace. The other tank was placed on the platform of the dial scales which gave continuous readings of the weight of that container. The bottom or #2 container was also connected to #1 container by 1/4" tubes through which the alloy could be forced from #2 to #1 container with the aid of moderate gas pressure. The 1/4 tubing was sealed off by a cold trap at the point shown as #3 on plate #1.

5. The capillary and return tubes were of such length and flexibility that weights of the order of 2 grams would cause a reflection on the dial scales. The dimensions of the capillary tube were 0.238 cm. inside diameter and 629 cm. in length.

6. The gas used in the viscosity studies was helium which had been purified by passing it over reduced copper at 450°C and then through reactivated charcoal at liquid nitrogen temperature.

B. Operation

7. From Plate 1, the operation of the unit was carried out as follows: The alloy was run through the valve #4 into container #2 until approximately 900 grams had entered the container. Valve #4 was then closed and helium pressure put on the #2 container through tube #5 which forced some gas back through the capillary tube, but at the same time exerted sufficient pressure on the alloy to cause it to flow through the cold trap (#4) into container #1. When #2 was nearly empty, as indicated by the scale reading, the pressure was released and the trap frozen in liquid nitrogen to form a seal against the return of the alloy by this route. The whole container and capillary tube were brought to desirable temperature and, with a pressure head adjusted to the desired value, the weight of the alloy which flowed through the capillary into container #2 was determined against time. The trap was then thawed and the operation repeated at various pressures and temperatures as desired.

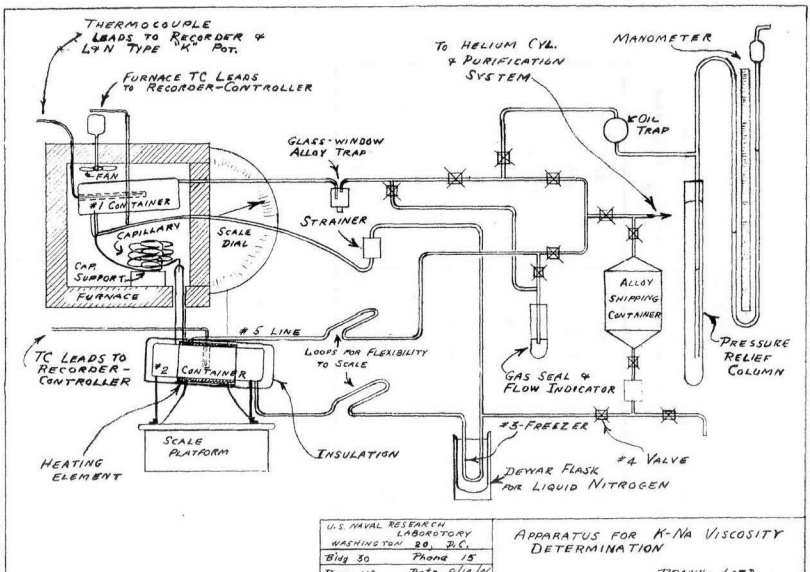
RESULTS

8. Measurements were made on water at 72°C with the pressure head at 6.65 cm. of Hg. This gave 1.374 grams (1.407 cc) of water per

second. Measurements were then made on the alloy over the temperature range. At the same pressure head and from a curve of grams of alloy per second against temperature, 1.110 grams of alloy flowed per second. This gave 1.267 as a relative viscosity of the alloy at 72°C. This value multiplied by 0.3952, the absolute viscosity of water, gives 0.501 as the absolute viscosity of the alloy at 72°C. Then with the constant determined as mentioned in paragraph 3, the absolute viscosity was caluclated at several temperatures over the range from 65.5°C to 700°C. The value for k was calculated as 0.5611 and the results on the viscosity are given in Table 1 and plotted on Plate 2. Along with this curve, values for pure sodium and potassium are given. These values were those published by Y.S. Chiong, Proc. Roy. Soc. London A157, 264(1936).

TABLE 1

Temperature °C	Volume cc/sec	Viscosity centipoises ±10%
65.5	1.093	.514
100	1.178	.476
200	1.415	.397
300	1.645	.341
400	1.855	.303
500	2.046	.274
600	2.193	.256
650	2.223	.252
700	2.167	.259



U.S. NAVAL RESEARCH LABORATORY WASHINGTON 20, D.C.	APPARATUS FOR K-Na VISCOSITY DETERMINATION
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P-2931

PLATE-1

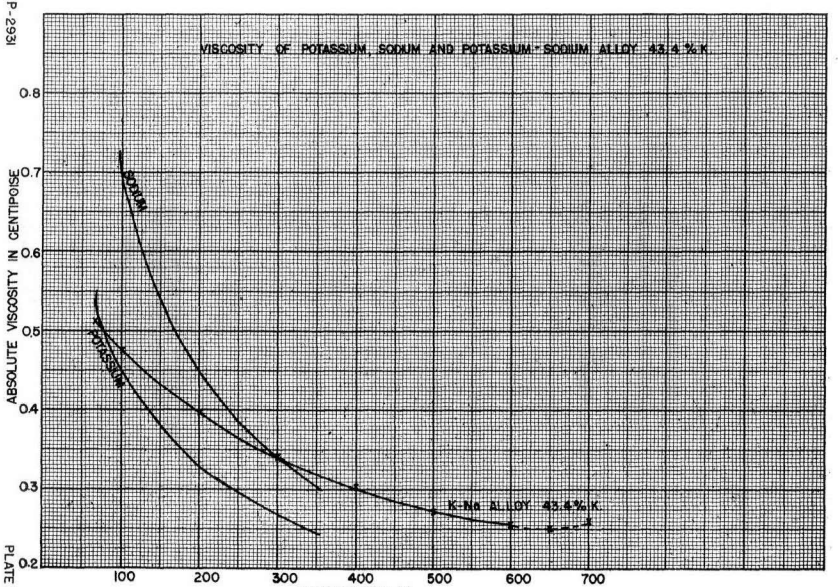

PLATE 2

P-2931

PRELIMINARY REPORT #1

DENSITY OF THE SYSTEM K-NA

by
C. B. Jackson
G. A. Wiesenreck and A. Van Andel

MINE SAFETY APPLIANCES COMPANY
Callery, Pennsylvania

October 1, 1946

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ABSTRACT

Measurements of the density of seven standard samples of K-Na alloys of various compositions were made and two density vs temperature °C curves are shown for each of the seven samples. Measurements of density from the melting point up to about 200°C were made using glass dilatometers, and from 300 to 700°C the density values were calculated from a measurement of the buoyancy of a copper plunger suspended in the various alloys. A series of curves show the variation of density with composition of alloy at 50° intervals from 0°C to 250°C and at 100° intervals from 300°C to 700°C. The 250°C curve data was extrapolated from the dilatometer data because it seemed to fit the density curves for each master sample better than extrapolated buoyancy data.

INTRODUCTION

A. Authorization

This project was carried out under Task Order I of Contract N6ori-146 dated 26 June 1946.

B. Statement of Problem

Contract calls for Laboratory Research necessary to arrive at satisfactory values for the physical properties of sodium and potassium alloys. The density has been determined on 7 standard samples of alloy. These values along with curves are supplied in this report. Composition-density isotherms permit the estimation of this density of any NaK alloy from melting point to 700°C with ± 0.5% accuracy.

C. Known Facts Bearing on the Problem

Two common methods of measuring the density of a homogeneous liquid are: (a) the measurement of the buoyant effect of liquid alloy on a plunger suspended in the alloy at different temperatures. (b) The measurement of the volume of a mass of the liquid in a dilatometer as it changes with temperature. This density is calculated from the equation $d = \frac{m}{v}$. Both methods were used at Mine Safety Appliances Company, method (a) at high temperature and method (b) at low temperature.

Two main difficulties to be encountered are the procurement of a good uniform sample that is representative of the master sample in the standard sample pot, and the prevention of any exposure whatsoever of the sample to oxygen or moisture during sampling and weighing or during the experiment while readings are being taken. It has already been demonstrated by Rinck that below 300 or 400°C it is very difficult to determine density by measuring buoyancy because of surface tension and other phenomena that limit sensitivity of the balance and prevent sufficient accuracy.

METHODS

A. Apparatus - High Temperature Measurements

An apparatus as shown in Plate 1 consisting of a nickel tube 15" long 1" inside diameter which contained an alloy sample approximately 5" deep was enclosed in an electrically heated, well-insulated furnace. The tube was closed at the top by a plug through which a brass tube was inserted (equipped with a side arm for nitrogen flow) and which permitted the passage of a plunger suspended by a nickel wire attached to a glass thread. The balance was placed on a table over the furnace, insulated against heat on the bottom. The suspension was made from the left hand pan down through a tiny hole drilled through pan, balance, and table. Power input to the furnace was regulated by a large rheostat. The temperatures were measured

by [illegible] the bottom of the [illegible] tube, and the other at the side of the tube at approximately the level of the alloy. The two temperatures were kept within 2°C in operation, and both were calibrated to read correctly to within .25°C. Correct freezing points were obtained with these thermocouples on known samples, which indicates that lag in temperature was negligible. The nitrogen was purified by a hot copper furnace at about 400°C, a CaCl2 tower and a P_2O_5 tower. At end of experiments the alloy was silvery on the surface after 10 to 15 hours.

B. Operation - High Temperature Measurements

The plunger was weighed in air to .0001 g. and its volume calculated by weighing while suspended in distilled water. Using density of water and copper from the handbook and coefficient of expansion of copper by Haring & Davy (Phys. Rev. 2-47 P 337 (1935) a value for the volume of the plunger at any temperature up to 700°C could be calculated. This value equals the volume of the alloy displaced. The weight of this displaced alloy was taken as weight of plunger suspended in air minus weight of plunger suspended in alloy. Corrections to weight in vacuum were considered negligible, since brass weights were used.

C. Apparatus - Low Temperature Measurements

Glass dilatometers used by Mine Safety Appliances Company were two pyrex dilatometers calibrated by Naval Research Laboratory and checked by Mine Safety Appliances Company. See Plate 2. They were cleaned carefully and weighed after each filling. No appreciable change in calibration took place since great care was exercised in preventing damage to the glass during testing. Dilatometers were clamped in a mineral oil bath heated by brass immersion heater with variac regulator and stirred constantly. Temperature was measured with thermometer calibrated by U. S. Bureau of Standards and accurate to 0.1°C. The bath varied about 0.1°C at points near the dilatometers. Readings were taken on heating only because the alloy wets the glass rather easily and prevents cooling and repetition of readings.

D. Operation - Low Temperature Measurements

Dilatometers were weighed in air suspended by a glass thread, and values were corrected to weighing in vacuo. They were flushed with nitrogen free from O_2 and H_2O. Alloy was introduced through a long capillary tube. Dilatometers were weighed again, the difference giving weight of alloy. Two samples of one alloy were run simultaneously and an analysis made for K content. The volumes of the dilatometers were corrected for thermal expansion using coefficient = 0.000025. Glass capillaries were used for alloys of low freezing point and copper capillaries were used for alloys of high freezing point.

RESULTS

At low temperatures duplicate runs were made on master samples 2, 3, 4, 5 and 6; one run was made on sample 1, and no runs were made on sample 7. It was found that the alloys richer in potassium generally wetted the glass dilatometers above 150°C rather easily with the slightest vibration and made it difficult to get readings. Results obtained on sample 3, the eutectic, were higher than would be expected if the density-composition curves were straight or nearly so, indicating that there may be a maximum in the curves in this range of composition. Results on samples 4 and 6 were lower than was expected and is believed to be due to occluded air bubbles in the dilatometer. Improved methods of filling the dilatometer and increasing the temperature range of available readings will provide abundant data for the next progress report, particularly on those of the master samples for which present data seems in any way unjustifiable. Probably the density-composition curves for 0 and 50°C should not be straight lines as shown on Plate 10.

At high temperatures it was found that alloys richer in potassium permitted more sensitivity in weighing the buoyancy of the plunger, and thus better density values were obtained below 400°C in the case of K or K-rich alloys. The data on pages 4 to 7 show the different runs as the temperature increased, and as it decreased for each run as long as the balance showed sensitivity.

In the table below, , is the coefficient of thermal expansion calculated from the straight line drawn from the dilatometer data at low temperatures, and is that for the buoyancy data at higher temperatures. Density figures for the temperature range above that covered by the dilatometer data and below that covered by the buoyancy data are obtained from the extension of the straight lines for each set of data until they intersect.

Coefficient of Cubical Expansion of NaK Alloys

$V = Vo(1 + T)$

Std. Spl.	T° Range	$_1 \times 10^4$	T° Range	$_2 \times 10^4$	Analysis % K
1	M.P. to 380	3.149	380 to 700	3.542	98.8
2	M.P. to 330	3.204	330 to 700	3.258	91.7
3	M.P. to 330	3.289	330 to 700	3.219	78.6
4	M.P. to 220	2.968	220 to 700	3.199	65.9
5	M.P. to 300	3.436	300 to 700	3.133	43.4
6	M.P. to 300	3.051	400 to 700	3.144	29.4
7	Not run at low temp.		400 to 700	3.459	0.2

Density Data for Standard Sample #1

T°C	Density
Dilatometer	
125	.8130
132	.8120
139.2	.8102
147	.8082
160	.8048
Buoyancy	
312	.769
358	.757
372	.751
405	.743
409	.741
455	.732
496	.721

T°C	Density
Buoyancy	
493	.721
550	.709
694	.676
693	.676
573	.706
544	.713
525	.718
495	.724
482	.728
461	.732
444	.737
398	.744
388	.750

Density Data for Standard Sample #2

Dilatometer	
85.5	.8294
94.4	.8271
101.0	.8255
108.0	.8239
115.5	.8219
123.0	.8200
131.0	.8180
138.0	.8162
144.0	.8138
151.2	.8129
156.0	.8116
115.5	.8255
123.0	.8234
131.0	.8215
138.0	.8197
144.0	.8183
151.2	.8164
157.6	.8149
165.2	.8130
171.4	.8114
178.5	.8097
185.0	.8081

Buoyancy	
340	.769
342	.767
341	.767
388	.756
399	.752
483	.733
506	.728
579	.713
581	.714
627	.704
671	.694
689	.690
694	.689
644	.701
606	.709
565	.720
532	.726
484	.739
434	.745
428	.750
420	.751

Density Data for Standard Sample #3

T°C	Density
Dilatometer	
112.3	.8442
122.0	.8421
127.5	.8404
135.2	.8385
142.3	.8366
149.0	.8349
157.0	.8328
164.5	.8309
171.1	.8293
178.2	.8274
184.8	.8259
196.7	.8225
204.0	.8206
Buoyancy	
404	.768
476	.756
515	.747
537	.739
579	.732
614	.724
651	.716
658	.715
641	.717
593	.719

T°C	Density
Buoyancy	
462	.760
500	.750
535	.740
566	.734
595	.728
620	.721
644	.716
678	.709
690	.705
700	.702
700	.702
699	.703
685	.708
672	.711
642	.718
616	.725
557	.735
550	.737
463	.758
389	.775
371	.779

Density Data for Standard Sample #4

Dilatometer	
63.6	.8656
67.7	.8646
66.2	.8650
72.0	.8635
79.1	.8615
81.0	.8609
86.0	.8595
92.0	.8578
98.6	.8559
105.5	.8543
112.7	.8542
120.0	.8523
126.8	.8505
161.8	.8468
169.1	.8447
175.8	.8429
181.7	.8410
188.3	.8391

Buoyancy	
510	.760
577	.745
672	.721
633	.736
534	.758
395	.790
465	.768
499	.762
562	.750
607	.740
658	.728
709	.719
704	.719
634	.738
532	.763
528	.766
429	.781
416	.783

LIBRARY
NAVAL RESEARCH LABORATORY

Density Data for Standard Sample #5

T°C	Density
Dilatometer	
23.8	.9119
25.2	.9109
26.7	.9113
49.8	.9029
86.0	.8937
23.8	.9083
25.2	.9087
26.7	.9082
49.8	.9024
85.0	.8929
110.3	.8816
119.6	.8795
127.2	.8775
134.5	.8756
142.0	.8735
148.8	.8717
155.8	.8698
163.5	.8680
172.0	.8658
95.9	.8867

T°C	Density
Dilatometer	
96.8	.8863
103.4	.8848
110.0	.8827
142.0	.8749
148.8	.8729
155.8	.8710
163.5	.8689
Buoyancy	
499	.7867
500	.787
566	.771
559	.771
635	.757
632	.756
699	.742
700	.742
582	.771
508	.788
447	.802
381	.813
350	.820

Density Data for Standard Sample #6

Dilatometer	
57.1	.9037
61.0	.9026
68.0	.9007
73.0	.8992
80.6	.8971
87.7	.8950
93.5	.8933
141.2	.8909
149.0	.8888
156.8	.8868
165.0	.8847
172.3	.8829
180.2	.8804
188.0	.8783
196.3	.8761
202.5	.8745
206.2	.8733
212.0	.8717

Buoyancy	
468	.820
466	.818
462	.819
512	.799
582	.785
585	.784
691	.760
678	.764
634	.773
573	.788
514	.802
478	.811
435	.816

Density Data For Standard Sample #7

T°C	Density
Buoyancy	
96	.938 (Backspill)
504	.838
540	.818
543	.817
595	.803
665	.786
712	.778
650	.792
601	.801
552	.811
503	.821

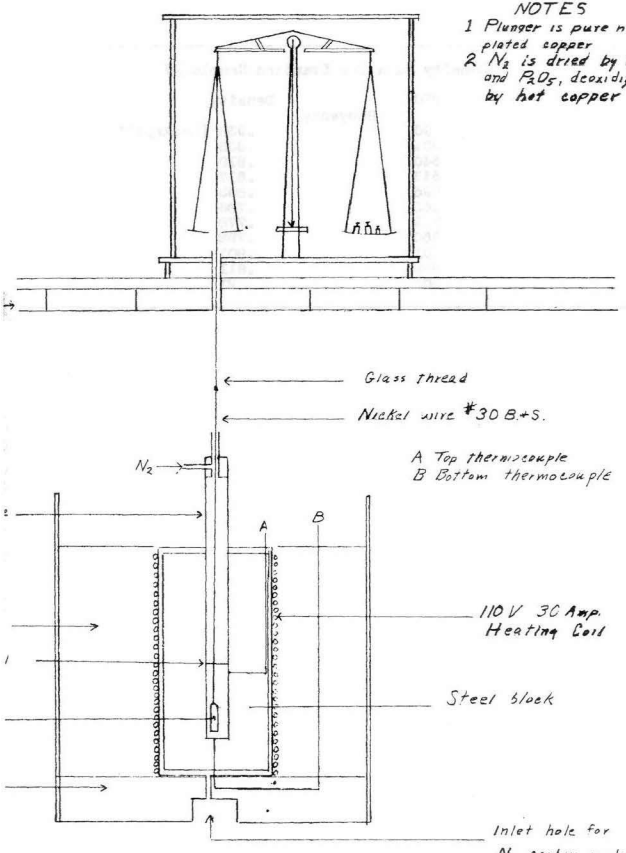
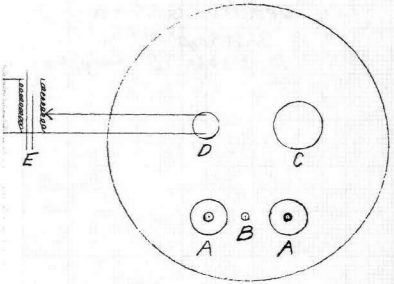


Plate 1

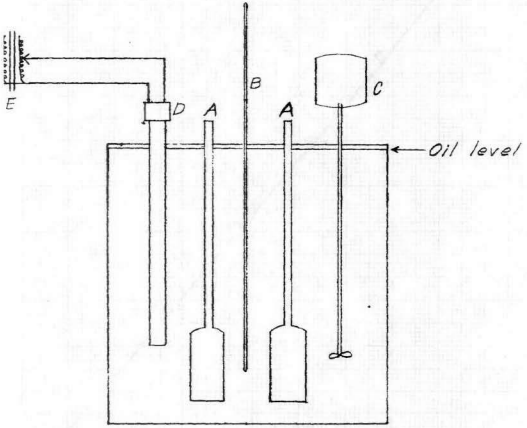
MINE SAFETY APPLIANCES CO.
CALLERY, PA.
KNA DENSITY APPARATUS
10-2-46 P.J.



NOTES

1. Apparatus located in top view.

A-Dilatometer
B-Thermometer
C-Stirrer
D-Immersion heater
E-Powerstat



MINE SAFETY APPLIANCES CO.
CALLERY, PA.
K-NA DENSITY APPARATUS
NO: 2
R.T. 10-3-46

Plate 2

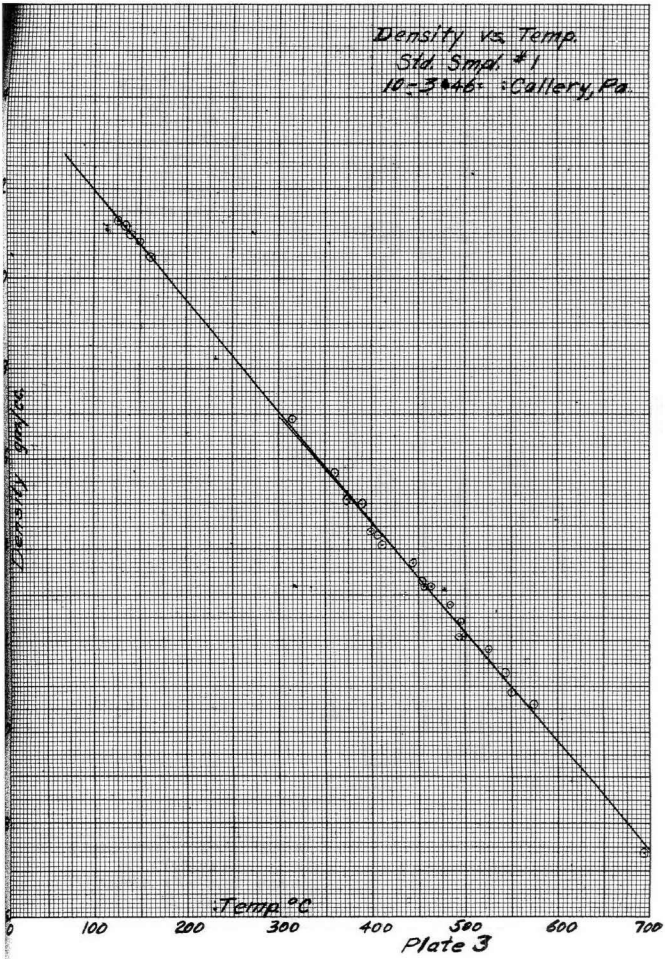

Density vs. Temp.
Std. Smpl. #1
10-3-46 : Callery, Pa.
Density gm/cc
Temp. °C
0
100
200
300
400
500
600
700

Plate 3

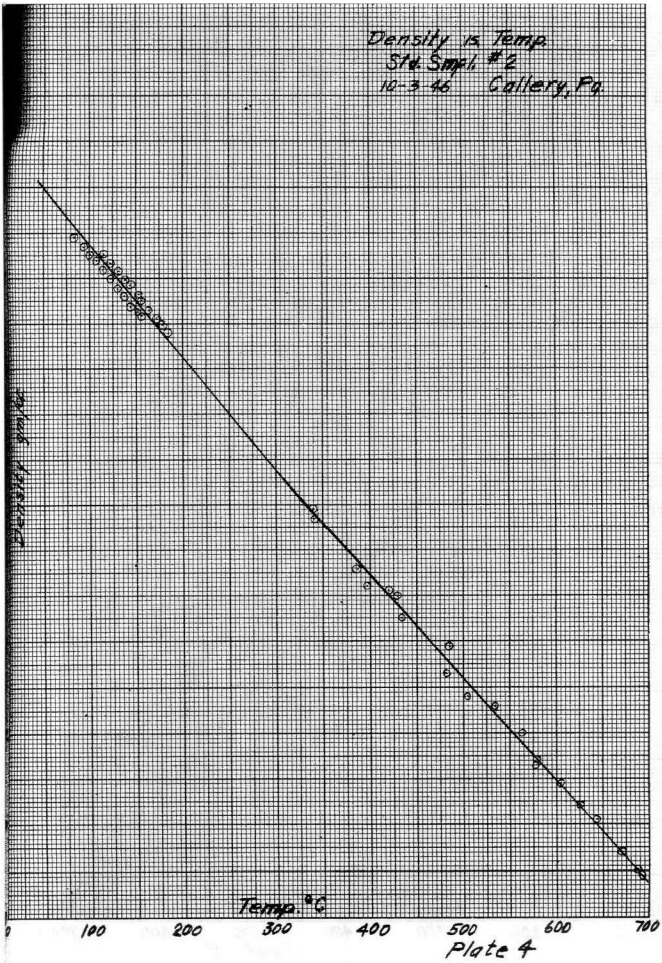

Density vs Temp.
Sta. Smpl. #2
10-3-46 Callery, Pa.
Relative Density
Temp. °C
0
100
200
300
400
500
600
700

Plate 4

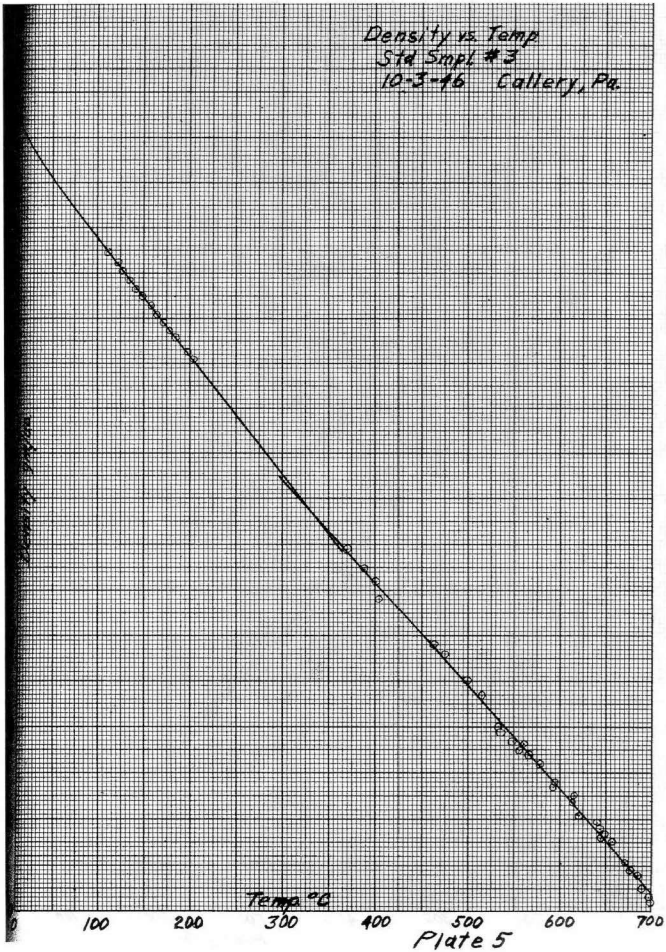

Density vs. Temp
Std Smpl #3
10-3-46 Callery, Pa.
Temp. °C
0
100
200
300
400
500
600
700

Plate 5

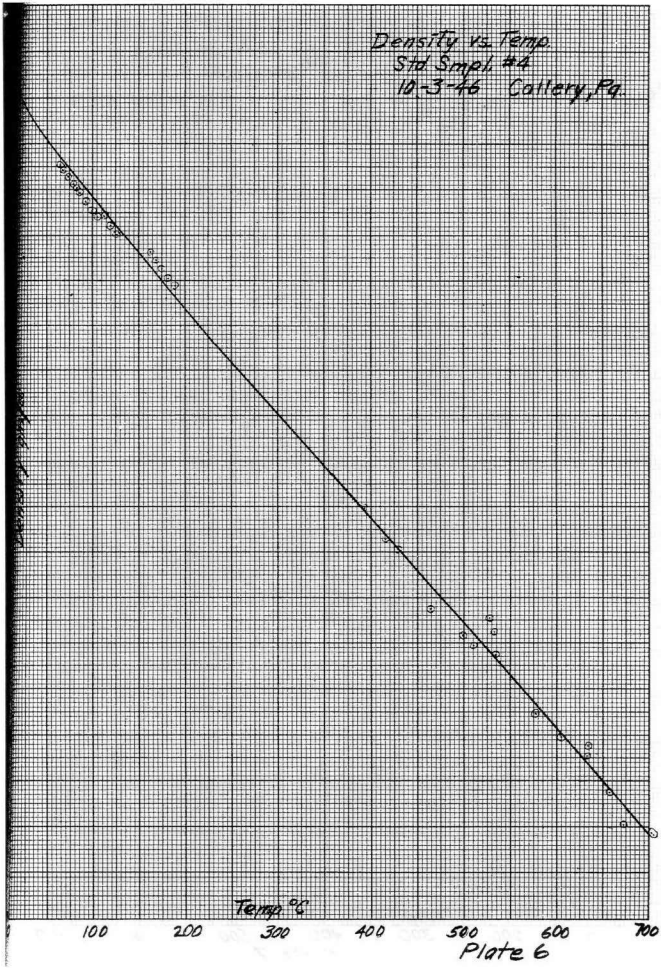

Density vs. Temp.
Std Smpl. #4
10-3-46 Callery, Pa.
Temp. °C
100
200
300
400
500
600
700

Plate 6

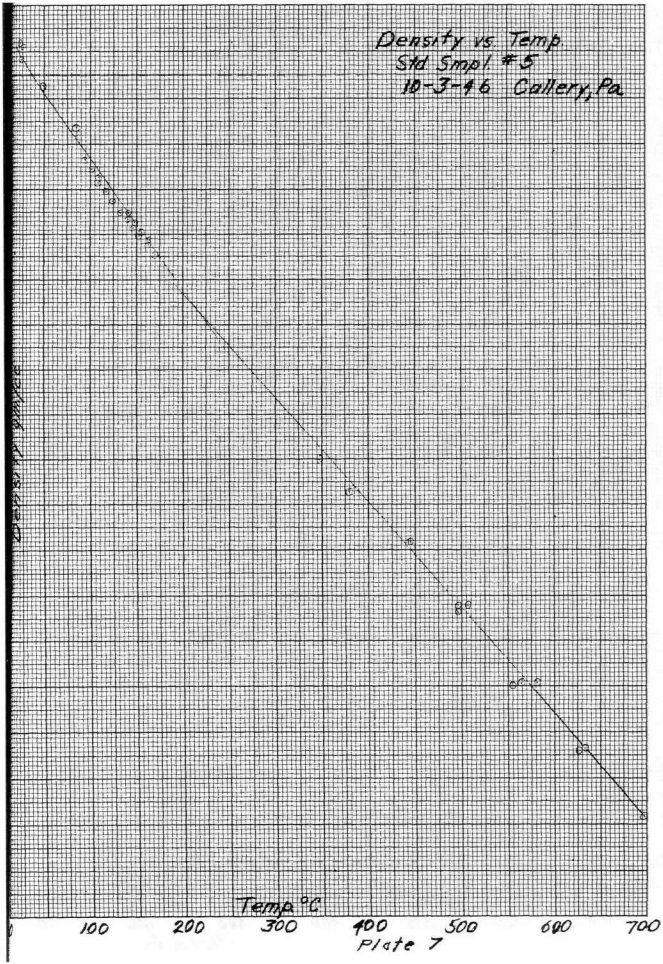

Density vs. Temp.
Std Smpl #5
10-3-46 Gallery, Pa.
Density gm/cm³
Temp °C
0
100
200
300
400
500
600
700

Plate 7

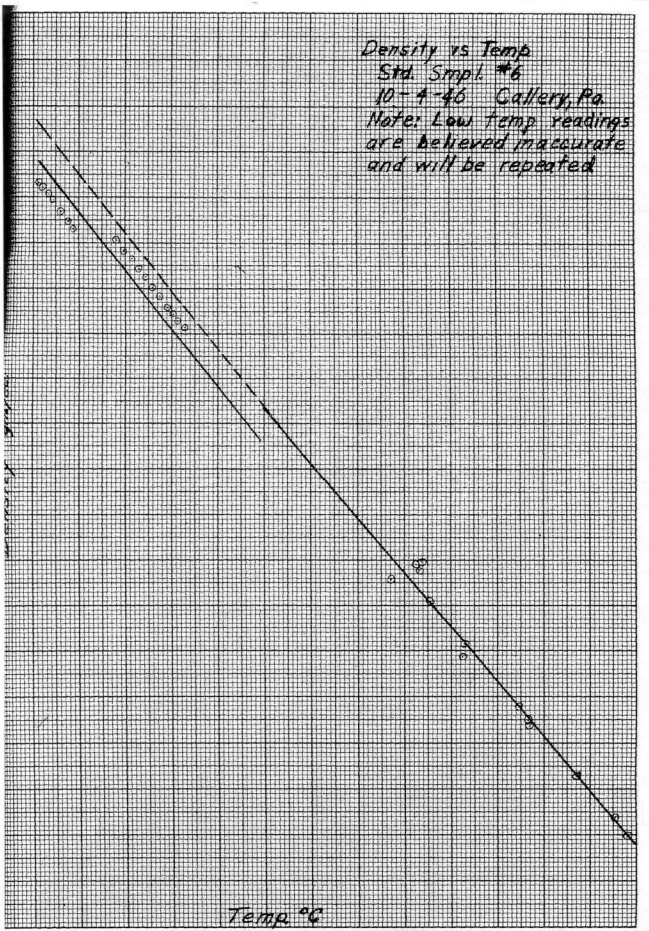

Density vs Temp
Std. Smpl. #6
10-4-46 Gallery, Pa.
Note: Low temp. readings are believed inaccurate and will be repeated
Temp. °C
100
200
300
400
500
600
700

Plate 8

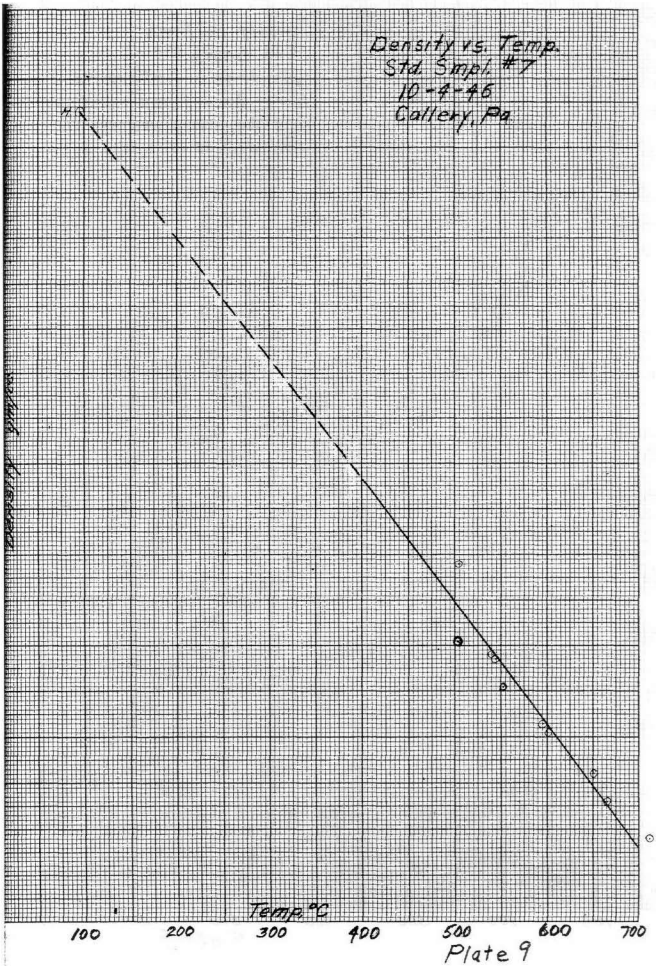

Density vs. Temp.
Std. Smpl. #7
10-4-46
Callery, Pa.
Density
Temp. °C
100
200
300
400
500
600
700

Plate 9

This report was received from the Argonne Laboratory, Chicago as report #CT3554. The work was done at the Battelle Institute, Columbus, Ohio)

REPORT

on

DETERMINATION OF THE THERMAL CONDUCTIVITY OF SODIUM-POTASSIUM ALLOY AT ELEVATED TEMPERATURES

Report prepared by: Herbert Deem
H. W. Russell

Classification changed
to NOT CLASSIFIED
Sept. 27, 1946
Authority of;DEMED

June 5, 1946

APPENDIX D

Contract No. W-7405-eng-92

REPORT

on

DETERMINATION OF THE THERMAL CONDUCTIVITY OF SODIUM-POTASSIUM ALLOY AT ELEVATED TEMPERATURES

Report prepared by: Herbert Deem
H. W. Russell

June 5, 1946

SUMMARY

The thermal conductivity of an alloy consisting of approximately 50 per cent sodium and 50 per cent potassium by weight was determined over a temperature range of approximately 100°C to 500°C. The thermal conductivity of the alloy in watts $cm.^{-2}$ $°C^{-1}$ was 0.258 at a mean temperature of 100°C. and 0.284 at a mean temperature of 500°C. The thermal conductivity increased linearly with temperature.

INTRODUCTION

The use of a sodium-potassium alloy as a coolant makes some knowledge of its thermal conductivity at various temperatures quite important. No such data were available, so a measuring technique was devised and suitable apparatus constructed. It was desired to make thermal-conductivity measurements at various temperatures to approximately 500°C., and this requirement restricted the methods available. An alloy of sodium and potassium is very active chemically, thus making important the choice of container material and handling technique.

The method selected and used for the determination of thermal conductivity was essentially that developed by the U. S.

Bureau of Standards and described in Research Papers RP668 and RP669. The method, in brief, consists of heating one end of a sample, measuring its temperature gradient, and determining the quantity of heat passing through it by means of a heat flowmeter consisting of a standard metal of known conductivity at the cold end. The sample and standard are surrounded by insulation and guard tube. When handling a liquid in such measurements, it is obviously necessary to provide a confining container and also to provide for an uninterrupted heat flow into and out of the container. Stainless steel (18-8) was used as a container as its conductivity (approximately 0.20 watts $cm.^{-1}$ $°C^{-1}$) is near that of the liquid.

APPARATUS

Figure 1 shows the apparatus used for thermal-conductivity measurements of the alloy. The over-all dimensions of the stainless-steel rod were 2 cm. in diameter and 15 cm. long to conform to the U. S. Bureau of Standards method. This rod was made in two pieces with an end of each hollowed to a depth of 1 cm. with wall 0.005 inch thick. A small lip was left on each wall to facilitate joining the pieces by means of a stainless-steel weld. After welding the pieces together, an alloy container was formed with dimensions 0.789 inch long and 0.777 inch in diameter. The 0.005-inch walls represented 2.5 per cent of the alloy cross-sectional area. A small hole, representing 1 per cent of the alloy area, was drilled into the specimen chamber for use in filling. A stainless-steel tube was welded to the top, which served as an expansion reservoir, and a small section

of steel tubing permitted making a flame seal after the assembly was filled with alloy.

Thermocouples of 36-gage chromel "P" and alumel wire were inserted as shown in Figure 1. Small pieces of stainless-steel tubing 0.020-inch O.D., (hypodermic needle stock), served to hold the beads firmly at the bottom of holes drilled into the stainless steel and Armco-iron standard. Locations of the thermocouple holes were determined by means of a comparator microscope.

A stainless steel-clad copper cylinder was tin-soldered to the upper end of the assembly and served to introduce heat from the furnace. The lower end of the assembly was tin-soldered to an Armco-iron standard cylinder which, in turn, was soldered to a water-cooled cap.

The furnace was designed according to U.S. Bureau of Standards specifications, but was used in an inverted position as shown in Figure 1. By introducing heat at the top and withdrawing it from the bottom, heat transfer through the alloy by convection will not occur. Three heating coils with individual controls made possible the introduction of the desired amount of heat into the copper cylinder, and also control of the guard-ring temperature. Large-capacity storage batteries were used to heat the furnace to secure constant heat input.

Temperatures were measured at 12 points, as shown in Figure 1. They included 5 points on the stainless-steel assembly, 2 points on the Armco-iron standard, and 5 points on the guard ring. Millivolt thermocouple readings were made on a Type K Leeds and Northrup potentiometer.

Cooling water was circulated from a thermostatically controlled tank constant to - 0.02°C at a rate of approximately 3.5 pounds per minute.

THE SODIUM-POTASSIUM ALLOY

Sodium and potassium of C.P. grade were melted individually under petroleum oil, and then pipetted into a weighed container of the same oil to make a 50-50 per cent by weight mixture. A chemical analysis of the alloy indicated its composition to be 51.7 per cent sodium and 48.3 per cent potassium.

A measured volume of 6.6 ml. was introduced into the specimen chamber which was sufficient to make the level approximately as shown in Figure 1. Radiographs were taken of the vertical assembly, both before and after the tests. These radiographs established the liquid level, and also showed that no significant voids existed at the upper alloy - stainless steel interface.

The stainless-steel assembly was evacuated to a pressure of less than 0.1 micron and filled by gravity flow from an evacuated vessel containing the liquid alloy.

RESULTS

Radial heat flow from the specimen assembly was made negligible by adjustment of the temperature of the guard tube. The temperatures of the upper and lower surfaces of the sodium-potassium alloy were determined by extrapolation of the measured temperature in the stainless-steel. This extrapolation was made in a nonlinear manner, allowing for the variation of the conductivity of stainless steel with temperature. The conductivity was com-

puted from the temperature gradient in the alloy and the rate of heat flow as indicated by the temperature gradient in the Armco-iron standard, and was referred to the mean temperature of the alloy. A correction, which was less than 1 per cent, was made for the effect of the stainless-steel walls of the specimen chamber. The computed results of all runs made are shown in Table 1.

Figure 2 shows a plot of the values given in Table 1.

As the cold end of the specimen assembly was maintained at the same temperature for all runs, the rate of heat flow increased specimen temperature. Thus, temperature gradients are larger and somewhat more accurately measurable at high specimen temperatures. The curve as given in Figure 2 (Curve a) was, therefore, drawn as a straight line, giving most weight to the high-temperature points. While the low-temperature points give some indication of curvature, this is at the limit of the precision of the method. Hornbeck[1] made thermal-conductivity measurements of an alloy with a composition of 63 per cent sodium and 37 per cent potassium by weight. His results are shown in Figure 2 (Curve b). Table 2 gives thermal-conductivity values taken from the line of Figure 2.

---

(1) Hornbeck, J. W., Thermal and Electrical Conductivities of the Alkali Metals, Physical Review 2, page 217, 1913.

TABLE 1. THERMAL-CONDUCTIVITY VALUES FOR SODIUM-POTASSIUM ALLOY OF COMPOSITION OF 51.7 PER CENT SODIUM AND 48.3 PER CENT POTASSIUM BY WEIGHT

Run	Mean Specimen Temperature, °C	Thermal Conductivity of Sodium-Potassium Alloy, Watts $cm.^{-2}$ cm. $°C.^{-1}$
1	211.3	0.254
2	297.7	0.274
3	496.5	0.282
4	441.6	0.278
5	379.8	0.276
6	223.7	0.261
7	222.6	0.263
8	216.1	0.271
9	142.6	0.249
10	139.0	0.245

TABLE 2. INTERPOLATED RESULTS OF THERMAL-CONDUCTIVITY VALUES FOR SODIUM-POTASSIUM ALLOY OF COMPOSITION OF 51.7 PER CENT SODIUM AND 48.3 PER CENT POTASSIUM BY WEIGHT

Mean Specimen Temperature, °C	Thermal Conductivity of Sodium-Potassium Alloy, Watts cm.$^{-2}$ cm. °C^{-1}
100	0.25_8
200	0.26_5
300	0.27_1
400	0.27_7
500	0.28_4

Note: 1 watt cm.$^{-2}$ cm. °C^{-1} = 0.239 cal. cm.$^{-2}$ cm.sec.$^{-1}$ °C^{-1}

HD:HWR/LM
June 12, 1946
copied 24 Oct.,46 EP

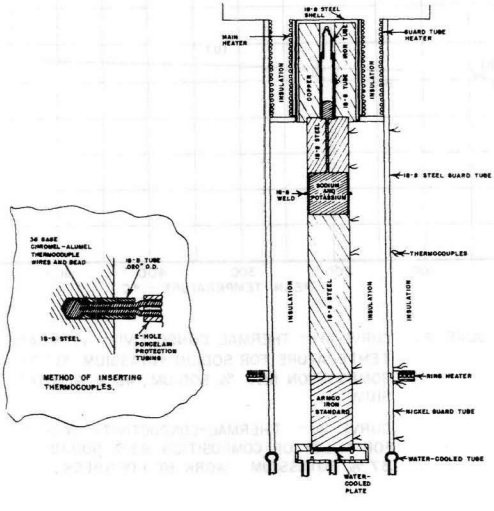


FIGURE 1. APPARATUS USED FOR THERMAL-CONDUCTIVITY DETERMINATION OF SODIUM AND POTASSIUM ALLOY.

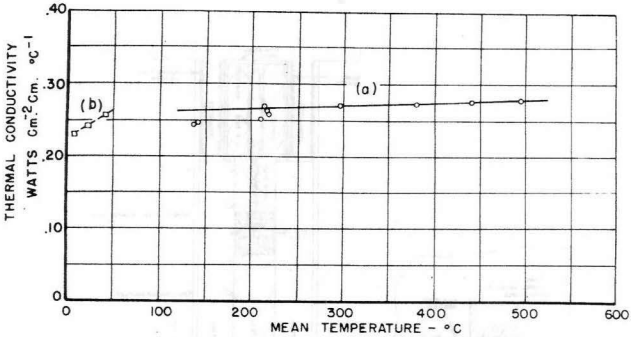


FIGURE 2. CURVE (a) - THERMAL CONDUCTIVITY vs. MEAN TEMPERATURE FOR SODIUM-POTASSIUM ALLOY. COMPOSITION 51.7 % SODIUM, 48.3 % POTASSIUM.

CURVE (b) - THERMAL-CONDUCTIVITY VALUES FOR ALLOY OF COMPOSITION 63 % SODIUM, 37 % POTASSIUM. WORK BY HORNBECK.

Navy Department - Office of Naval Research

Naval Research Laboratory
Washington, D. C.

* * *

CHEMISTRY DIVISION

10 April 1941

Report on VAPOR-LIQUID EQUILIBRIA for MIXTURES of ALKALI METALS. (SODIUM-POTASSIUM)

by
NDRC - DIVISION B
for the
Naval Research Laboratory

- Report P-2958 -

* * *

Approved by:

Dr. P. Borgstrom
Superintendent,
Chemistry Division.

Commodore H. A. Schade, USN
Director,
Naval Research Laboratory.

Preliminary Pages. . . . . a-d
Numbered Pages 7
Plates 2

NATIONAL DEFENSE RESEARCH COMMITTEE

DIVISION B

Final Report on "Vapor-Liquid Equilibria for Mixtures of Alkali Metals"

Serial No. 22

Copy No. 7

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NATIONAL DEFENSE RESEARCH COMMITTEE

DIVISION B

Section L-6

Report on "Vapor-Liquid Equilibria for Mixtures of Alkali Metals"

Endorsement (1) from G. B. Kistiakowsky, Official Investiga tor, to W. K. Lewis, Vice-Chairman, Division B. Forwarding report.

(2) from W. K. Lewis, Vice-Chairman, Division B to J. B. Conant, Chairman, Division B. Forwarding report and noting:

> "This report supplies the data requested by the Naval Research Laboratory for use in connection with their study of the manufacture of potassium peroxide."

(3) Six copies forwarded to Dr. Irvin Stewart, Secretary of the National Defense Research Committee, as Final Report under Contract (b-24, NDCrcll) with Harvard University. Division B, Serial No. 22

/s/ J. B. Conant, Chairman
by Harris M. Chadwell

SUMMARY

Vapor-liquid equilibrium data for the system sodium-potassium at one atmosphere have been determined experimentally, and the results are tabulated in the attached Table I.

THE LIQUID-VAPOR EQUILIBRIUM IN BINARY SODIUM-POTASSIUM MIXTURES AT ATMOSPHERIC PRESSURE.

This final report on the liquid-vapor equilibria in the sodium-potassium system has been somewhat delayed because of several difficulties encountered in developing the technique for accurate equilibrium measurements. Mainly, the difficulties were:

1. The temperatures at which the alkali metals boil at atmospheric pressure are so high that glass equipment can not be used, and fused quartz is too rapidly attacked to be employed. The entire apparatus was constructed therefore of steel. In view of some information in the literature that alkali metals dissolve the constituents of stainless steels, ordinary mild carbon steel was used for the first two designs. Our experience has shown, however, that mild steel is so rapidly oxidized at the high temperature in question that the units become unserviceable before many measurements can be completed. Ordinary steel had to be discarded therefore, and a third unit was build of the 18-8 stainless steel. The constancy of the boiling points observed with this apparatus and the agreement of the observed boiling point of potassium with that recorded in the literature indicated that under our conditions the dissolving action of the alkalis was negligible.

2. Very extensive superheating of the molten metals occurred under conditions of our experiments and some difficulty was encountered in overcoming this phenomenon.

(copy of OSRD report, Ser. 22)

High surface tension of the molten metals causes considerable inconvenience in manipulations on a small scale.

Purification of Materials

Best commercially available grades of alkali metals packed in kerosene were used. Under an atmosphere of carbon dioxide, each stick was dried with filter paper and the outer crust cut away. The final traces of kerosene were removed by washing with benzene. The alkalis were then purified in an all-glass apparatus by high vacuum distillation; the distillation temperature for sodium was 500°C and for potassium it was 400°C. The sodium was collected in a number of glass tubes of about 10 cc. capacity, each tube being successively sealed off. The bottom of each glass tube had been previously blown into a thin-walled bulb which could be broken at the appropriate time. Similarly, 100 cc. of potassium was distilled into a flask provided also with a thin-walled bulb.

Apparatus and Procedure

The still for the determination of the liquid-vapor equilibrium is schematically shown in Figure 1. The entire still was made of stainless steel and all the joints were hydrogen-welded. After adequate baking out at 900°C the still could be evacuated to 10^{-4} mm. pressure at this temperature and maintained this vacuum for several hours.

The top, main body, and bottom of the still was heated separately. The top and the main body heaters were made of No. 18 Chromel-A wire, insulated by 1/8" porcelain beads. Platinum wire No. 22 was used for the bottom heater and was also insulated

by porcelain beads. Sil-O-Cell bricks, 3/4" thick and carved to fit the apparatus, provided the heat insulation. In operation the main body and the bend of the still were maintained at a slightly higher (10°) temperature than that of the boiling metal and the entire condensation occurred in Section C, the cooling agent being air, blown through the Jacket D. The air stream was so regulated that the temperature of condensed metal in Section B in the various experiments was between 150°C and 170°C.

When a steady state was reached, the Receiver E contained a few cc. of molten metal of the same composition as that of the vapor and the excess was being returned to the pot by the overflow Tube F. In order to keep the metals boiling steadily it was found necessary to pass a slow stream of nitrogen under the surface of the liquid by means of Tube B. This tube was connected to a source of carefully purified nitrogen, from which the last traces of oxygen were removed by bubbling it through a liquid eutectic mixture of sodium and potassium. Otherwise superheating by as much as 100° occurred, followed by explosion-like boiling. The volume of nitrogen passed was so small as not to affect appreciably the partial pressures of the metals (about 6cc. of nitrogen against some two to three liters of metallic vapors per minute).

The temperature of the boiling metal was measured by a platinum-rhodium thermocouple, protected by a quartz tube and placed in the Well A, which reached within 2 cm. of the surface of the liquid. It was experimentally found that displacements of the couple in the well, changes of the heating current through the main body heater, changes of the heating current (and there-

fore of the rate of boiling) of the bottom heater and changes of the rate of bubbling of nitrogen, had no effect upon the temperature recorded by the thermocouple when pure potassium was used in the boiling pot. The thermocouple was calibrated at the melting points of a Bureau of Standards sample of aluminum (m.p.= 660.15°C), and an analytical reagent grade of silver (m.p.=960.5°C). A Chromel-Alumel thermocouple was used to measure the temperature in Well-A'.

To maintain constant pressure during boiling, a 64 liter tank containing highly purified nitrogen at 76 cm. pressure was connected to the still. The inside surface of the connecting tube was covered with freshly distilled potassium metal to prevent the last traces of oxygen and mercury vapor from reaching the still.

Before filling the still with alkali metals it was heated to 800°C and hydrogen passed through it to reduce metallic oxides formed in the process of welding.

Metallic potassium and sodium were introduced into the still through the Needle Valve G, by means of a glass apparatus which fitted vacuum-tight to the ground joint K, a special cement (Shawinigan resin, m.p. 55°C) was used as the lubricating agent. The filling operation was completely carried out in an atmosphere of pure nitrogen so that the metals remained free of oxides. The Ground joint K and a similar one attached to the Needle Valve H fitted also multiple glass receivers into which 1/2 gram samples of liquid metal were withdrawn in the absence of air after a stationary state of boiling had been reached. The samples withdrawn at K gave the composition of the liquid

and those at H, the composition of the vapor. Before each withdrawal a small quantity of metal was sucked out of the Needle Valves to flush them.

From the heats of vaporization of the two alkalis and the energy input into the bottom heater, the boiling rates were computed to be from .5 to 1.5 cc. of liquid metal per minute. After the start of boiling approximately three hours were allowed for the establishment of a stationary state before the first sample was withdrawn. The next sample followed an hour and a half to two hours later and an equal time interval elapsed before a third sample was taken. The first measurement was made using the available 100 g. sample of pure potassium. Before each successive point on the composition diagram was obtained, some molten metal was withdrawn from the apparatus and an approximately equal amount of sodium introduced. From the start to the finish of the final series of experiments here described, air was not admitted to the system.

The method of analysis was as follows: first, a sample of approximately .5 gm. of the sodium-potassium mixture was converted to the hydroxides by the addition of absolute ethyl alcohol and then of 50 cc. of water. An aliquote part of this solution was transferred to a weighed glass evaporating dish and titrated with 0.15N HCl using methyl orange as the indicator. The resulting solution was evaporated to dryness in an oven at 110°C; in order to remove the final traces of water, the dish was placed in another oven at 160°C for five hours and then heated to 300° for 15 minutes. It was then weighed, reheated and reweighed again.

The weight of the resulting chlorides and the volume of

the acid used enabled one to compute the mole fractions of sodium and potassium in the sample. By analyzing known mixtures, this method has been found to be accurate to .005 in mole fractions.

Experimental Results

The experimental data are collected in Table I. A plot of the experimental points on a large-scale temperature-composition graph shows that smooth curves can be drawn with individual points deviating from the curves by less than 1° temperature or 1 mole per cent composition. Such scattering is accounted for by the previously mentioned analytical errors and by random fluctuations of temperature during boiling, which normally amounted to less than 1°C. The fluctuation was due chiefly to the irregular manner in which the condensed liquid was returned to the boiling pot through Tube F. The very high surface tension of the liquid metals accounts probably for this irregularity.

The results seem to indicate that some deviations from ideal liquid mixtures exist in the sodium-potassium system. These deviations are in a direction bringing the vapor and the liquid compositions closer together. Quite likely the deviations are due to the formation in the mixed vapor of the molecules, KNa, in addition to the molecules K_2 and Na_2.

Since the equilibrium constants of the gaseous reactions $2\ K = K_2$; $K + Na = KNa$; $2\ Na = Na_2$ can be accurately calculated from the available spectroscopic data, it should be possible to calculate theoretically the deviations from ideal mixture laws for the potassium-sodium system. Such calculations may be

profitable if information for several boiling pressures is wanted.

TABLE I

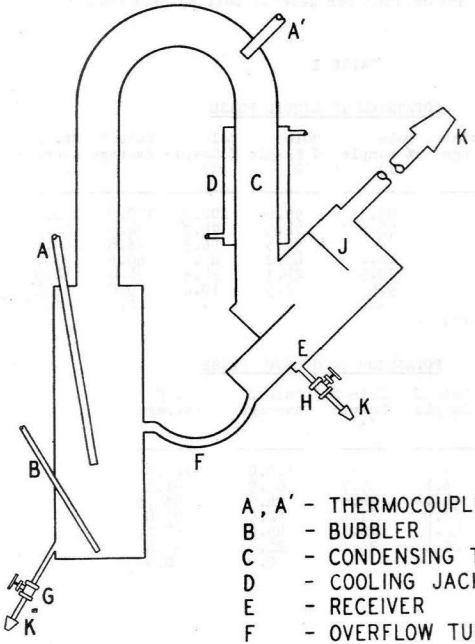
POTASSIUM IN LIQUID PHASE

Boiling Point in °C Average	Mole % Sample (1)	Mole % Sample (2)	Mole % Sample (3)	Mole % Average	Wt. % Average
757	99.5	99.4	100.7	100.0	100.0
778	74.9	74.4	74.7	74.5	83.3
796	-	57.3	56.2	56.8	69.1
814	40.2	41.2	40.5	40.6	53.7
835	23.5	21.3	24.2	24.0	34.9
858	9.5	9.5	10.4	9.8	15.6
(882 Literature)	-	-	-	0.0	0.0

POTASSIUM IN GASEOUS PHASE

Mole % Sample (1)	Mole % Sample (2)	Mole % Sample (3)	Mole % Average	Wt. % Average
-	-	-	100.0	100.0
	86.1	85.7	85.9	91.3
-	74.2	74.8	74.5	83.3
63.5	62.5	61.6	62.5	73.8
45.4	44.5	45.1	45.0	58.1
23.0	22.3	23.1	22.8	33.4
-	-	-	0.0	0.0

(copy of OSRD report, Ser. 22)



A, A' - THERMOCOUPLE WELLS
B - BUBBLER
C - CONDENSING TUBE
D - COOLING JACKET
E - RECEIVER
F - OVERFLOW TUBE
G, H - NEEDLE VALVES
J - GUARD
K - GROUND JOINTS

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PLATE I

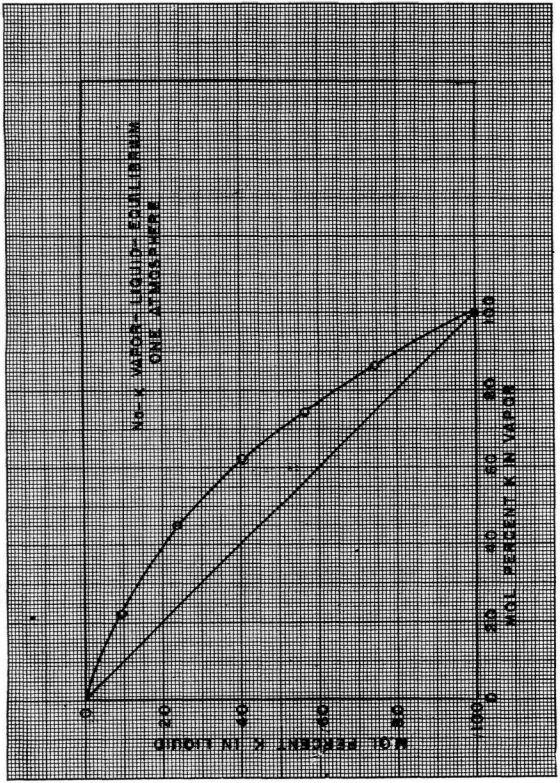

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PLATE 2

PRELIMINARY REPORT #2

THEORY OF "FIGURE OF EIGHT" HEAT EXCHANGER

by

W. L. McCabe and R. A. Tidball

MINE SAFETY APPLIANCES COMPANY
Callery, Pennsylvania

October 1, 1946

APPENDIX F

ABSTRACT

A double pipe, counter current, heat exchanger has been installed to measure heat transfer coefficients of the various KNa alloys. A method of calculation has been devised to determine these coefficients and to study the effects of the low value of the Prandtl Number.

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B. Statement of Problem.....1
C. Known Facts Bearing on the Problem...1

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Plate 1

PREVIOUS REPORTS

#1 - DENSITY OF SYSTEM K-NA

INTRODUCTION

A. Authorization

1. This work was authorized by Contract No. N6ori-146.

B. Statement of Problem

2. The project covers the engineering research necessary to determine heat transfer values of KNa alloys. Values will be determined on the seven standard samples in this apparatus.

C. Known Facts Bearing on the Problem

3. Heat transferred from a moving fluid to a solid is retarded by a fluid film at the liquid-solid interface. The resistance can be measured experimentally either by measuring the temperature of the metal wall, or indirectly through the use of the equations derived in this report. The resistance of an individual film depends upon two dimensionless groups - the Reynolds Number and the Prandtl Number. The effect of the former is well-known, but the Prandtl number of KNa alloys is much lower than those of the fluids normally used in heat transfer work, and the effect of such very low Prandtl numbers is unknown. The method used in this work is designed to isolate the Prandtl number factor.

NOMENCLATURE

A_i = Area of inside of inner tube.

q_i = Heat flow rate through wall of inner tube.

h_i = Heat transfer coefficient, warm fluid to inside surface of inner tube.

h_o = Heat transfer coefficient, outside of inner tube to cold fluid.

D_o = Outside diameter of inner tube.

D_i = Inside diameter of inner tube.

D_{av} = Average diameter of inner tube.

D_e = Equivalent diameter of annulus.

D_a = Inside diameter of outer tube.

k_w = Thermal conductivity of inner tube.

C_p = Specific heat of fluid.

G_i = Mass velocity of fluid through inner tube.

G_o = Mass velocity of fluid through outer tube.

L = Heated length of inner tube.

F = Prandtl Number function.

μ_i = Viscosity of fluid in inner tube.

μ_o = Viscosity of fluid in outer tube.

k = Thermal conductivity of fluid.

β = G_i/G_o

V = Mass flow rate.

N_{re} = $\frac{DG}{\mu}$ = Reynolds Number

N_{pr} = $\frac{C_p\mu}{k}$ = Prandtl Number

U = Overall coefficient of heat transfer from warm fluid through inner tube to cold fluid.

heory of the "Figure of Eight" Double Pipe

Counter Current Heat Exchanger

asic Equations (clean tubes)

$q_i = UA_i \Delta t_m$ M&Adams (16) p. 142

$$U = \frac{q_i}{A_i \Delta t_m}$$

$$\frac{1}{U} = \frac{1}{h_i} + \frac{x_w}{K_w} + \frac{1}{h_o}$$ M&Adams (7b) p. 136

Since $x_w = \frac{(D_o - D_i)}{2}$ and the ratio $\frac{D_i}{D_{av}}$ refers the resistance K_w to the inside wall, and the ratio $\frac{D_i}{D_o}$ refers the resistance h_o to the inside wall. these values can be introduced into (b) and (e)

$$\frac{\Delta t_m A_i}{q_i} = \frac{1}{h_i} + \frac{(D_o - D_i)\left(\frac{D_i}{D_{av}}\right)}{2 K_w} + \frac{\left(\frac{D_i}{D_o}\right)}{h_o}$$

Assuming C_p Constant

$$q_i = G_i C_p (t_{i1} - t_{i2}) \left(\frac{\pi}{4}\right)(D_i)^2$$

$$A_i = \pi D_i L$$

Assume

$$h_i = F G_i C_p \left(\frac{D_i G_i}{\mu_i}\right)^{-0.2}$$

$$h_i = F G_i^{.8} C_p \left(\frac{\mu_i}{D_i}\right)^{.2}$$ M&Adams (7) p. 182

d.

$$h_o = 0.87\left(\frac{D_a}{D_o}\right)^{0.53} F\, G_o\, C_p \left(\frac{D_e G_o}{\mu_o}\right)^{-0.2}$$ M&Adams (25a) p.202

$$0.87 = \frac{0.020}{0.023}$$

Where $F = N_{pr}$ function

r calculation assume

$$F = \frac{0.023}{0.05 + (N_{pr})^{2/3}}$$ MS Adams p. 197 for liquids with low N_{pr}

sume N_{pr} constant so F is same for

th streams.

Let $\beta = \frac{G_i}{G_o}$

nere $\beta = \frac{\text{Transverse area of annulus}}{\text{Transverse area of tube}}$

troducing 2, 3, 4, 5, and 7 into 1

$$\frac{t_m \pi D_i L}{C_p (t_{i1} - t_{i2}) \pi (D_i)^2} = \frac{1}{F (G_i)^{0.8} C_p \left(\frac{\mu_i}{D_i}\right)^{0.2}} + \frac{(D_o - D_i)(D_i)}{2 K_w D_{av}} + \frac{D_i \beta}{0.87\, D_o \left(\frac{D_a}{D_o}\right)^{0.53} G_i\, C_p \left(\frac{D_e G_o}{\beta \mu_o}\right)^{-0.2}}$$

nee $D_{av} = \frac{D_i + D_o}{2}$ and $D_e = D_a - D_o$

$$\frac{4\Delta t_m\left(\frac{L}{D_i}\right)}{G_i\, C_p\,(t_{i1}-t_{i2})} = \frac{1}{F(G_i)^{0.8}\, C_p\left(\frac{\mu_i}{D_i}\right)^{0.2}} + \frac{(D_o-D_i)(D_i)}{K_w(D_o+D_i)}$$

$$+ \frac{\beta\, D_i}{0.87\, D_o\left(\frac{D_a}{D_o}\right)^{0.53}(G_i)^{0.8}\, C_p\left(\frac{\mu_o}{D_a-D_o}\right)^{0.2} F}$$

$$\frac{4\Delta t_m\left(\frac{L}{D_i}\right)}{(t_{i1}-t_{i2})} = \frac{G_i^{0.2}}{F}\left[\left(\frac{D_i}{\mu_i}\right)^{0.2} + \frac{\beta^{0.8}(D_a-D_o)^{0.2}\left(\frac{D_i}{D_o}\right)}{(\mu_o^{0.2})\,0.87\left(\frac{D_a}{D_o}\right)^{0.53}}\right]$$

$$+ \frac{G_i\, C_p\, D_i(D_o-D_i)}{K_w(D_o+D_i)}$$

Introducing Reynolds number

$$N_{Rei} = \frac{D_i G_i}{\mu_i}$$

$$\frac{4\Delta t_m\left(\frac{L}{D_i}\right)}{(t_{i1}-t_{i2})} = \frac{1}{F}\left(\frac{N_{Rei}\,\mu_i}{D_i}\right)^{0.2}\left[\left(\frac{D_i}{\mu_i}\right)^{0.2} + \frac{\beta^{0.8}(D_a-D_o)^{0.2}\left(\frac{D_i}{D_o}\right)}{0.87(\mu_o)^{0.2}\left(\frac{D_a}{D_o}\right)^{0.53}}\right]$$

$$+ \frac{C_p\, N_{Rei}\,\mu_i\left(\frac{D_o}{D_i}-1\right)}{K_w\left(\frac{D_o}{D_i}+1\right)}$$

$$\frac{4\Delta t_m\left(\frac{L}{D_i}\right)}{(t_{i1}-t_{i2})} = \frac{N_{Rei}}{F}\left[1+\left(\frac{\mu_i}{\mu_o}\right)^{0.2}\frac{\beta^{0.8}(D_a-D_o)^{0.2}\left(\frac{D_i}{D_o}\right)}{0.87\left(\frac{D_a}{D_o}\right)^{0.53}(D_i)^{0.2}}\right]$$

$$+ \frac{N_{Rei}\,\mu_i\, C_p\left(\frac{D_o}{D_i}-1\right)}{K_w\left(\frac{D_o}{D_i}+1\right)}$$

Since $\beta = \dfrac{(D_a)^2 - (D_o)^2}{(D_i)^2}$

$$\frac{\beta^{0.8}(D_a - D_o)^{0.2} D_i}{(D_i)^{0.2}(D_o)} = \left[\frac{(D_a)^2 - (D_o)^2}{(D_i)^2}\right]^{0.8} \frac{(D_a - D_o)^{0.2} D_i}{(D_i)^{0.2} D_o}$$

$$= \frac{(D_a + D_o)^{0.8}(D_a - D_o)^{0.8}(D_a - D_o)^{0.2} D_i}{(D_i)^{1.6}(D_i)^{0.2}(D_o)}$$

$$= \left(\frac{D_a + D_o}{D_i}\right)^{0.8}\left(\frac{D_a - D_o}{D_o}\right)$$

$$= \left(\frac{D_a}{D_i} + \frac{D_o}{D_i}\right)^{0.8}\left(\frac{D_a}{D_o} - 1\right)$$

12) $$\frac{4\Delta t_m \left(\frac{L}{D_i}\right)}{(t_{i1} - t_{i2})} = \frac{N_{Rei}}{F}\left[1 + \left(\frac{\mu_i}{\mu_o}\right)^{0.2} \frac{\left(\frac{D_a}{D_i} + \frac{D_o}{D_i}\right)^{0.8}\left(\frac{D_a}{D_o} - 1\right)}{0.87\left(\frac{D_a}{D_o}\right)^{0.53}}\right] + \frac{N_{Rei}\,\mu_i\, C_p\left(\frac{D_o}{D_i} - 1\right)}{K_w\left(\frac{D_o}{D_i} + 1\right)}$$

or

13) $$F = \frac{(N_{Rei})^{0.2}\left[1 + \left(\frac{\mu_i}{\mu_o}\right)^{0.2} \frac{\left(\frac{D_a}{D_i} + \frac{D_o}{D_i}\right)^{0.8}\left(\frac{D_a}{D_o} - 1\right)}{0.87\left(\frac{D_a}{D_o}\right)^{0.53}}\right]}{\frac{4\Delta t_m\left(\frac{L}{D_i}\right)}{(t_{i1} - t_{i2})} - \frac{N_{Rei}\,\mu_i\, C_p\left(\frac{D_o}{D_i} - 1\right)}{K_w\left(\frac{D_o}{D_i} + 1\right)}}$$

This value of F is used in equations #4 and #5 to determine h_i and h_o

METHODS

A. Apparatus

4. An apparatus shown on Plate 1 was constructed to collect experimental data to determine heat transfer coefficients of NaK alloys. The test section (B) was 22" between thermocouples and constructed of mild steel tubing. The inner tube has an inside diameter of 0.402" and an outside diameter of 0.50". The outer tube has an inside diameter of 0.87" and an outside diameter of 1.00". Temperatures t_{i1}, t_{i2}, t_{o1} and t_{o2} are read on a Leeds and Northup Portable Precision potentiometer with iron-constantan thermocouples and an ice water cold junction. The alloy was heated by a 2000 watt immersion heater (A) controlled by a powerstat. Flow was measured with an inclined mercury and a calibrated orifice (F). Neo hexane was used to seal the alloy from the mercury. Flow was controlled by a valve (D) between the Worthington 3X $\frac{1}{2}$ Gear pump (G) and the annulus (C). A secondary double pipe heat exchanger (G) was used to cool the alloy. The surge tank (E) was used to absorb expansion of the alloy.

Design of exchangers for higher temperatures will be based on data obtained from this apparatus.

Sample calculations based on assumed data follows.

Sample Calculations

$V = 2200$ lbs./hr.
$\Delta t_m = 7.25$ °F
$t_{i_1} - t_{i_2} = 2.60$ °F
$L = 22''$
$D_a = 0.87''$
$D_o = 0.50''$
$D_i = 0.402''$
$\mu_i = \mu_o = 1.283$ lbs./(ft.)(hr.)
$C_p = 0.27$ Btu./(lb.)(°F)
$K_w = 26$ Btu./(hr.)(ft.^{2})(°F/ft.)
$\beta = 3.14$
$G_i = 2{,}500{,}000$ lbs./(hr.)(ft.^{2})
$G_o = 795{,}000$ lbs./(hr.)(ft.^{2})
$N_{Rei} = 65{,}400$
$N_{Reo} = 19{,}100$

$$F = \frac{(N_{Rei})^{0.2}\left[1+\left(\frac{\mu_i}{\mu_o}\right)^{0.2}\frac{\left(\frac{D_a}{D_i}+\frac{D_o}{D_i}\right)^{0.8}\left(\frac{D_a}{D_o}-1\right)}{0.87\left(\frac{D_a}{D_o}\right)^{0.53}}\right]}{\frac{4\,\Delta t_m\left(\frac{L}{D_i}\right)}{(t_{i_1}-t_{i_2})} - \frac{(N_{Rei})\,\mu_i\,C_p\left(\frac{D_o}{D_i}-1\right)}{K_w\left(\frac{D_o}{D_i}+1\right)}}$$

$$= \frac{(65{,}400)^{0.2}\left[1+(1)^{0.2}\frac{\left(\frac{0.87}{0.402}+\frac{0.50}{0.402}\right)^{0.8}\left(\frac{0.87}{0.50}-1\right)}{0.87\left(\frac{0.87}{0.50}\right)^{0.53}}\right]}{\frac{4(7.25)\left(\frac{22}{0.402}\right)}{2.60} - \frac{(65{,}400)(1.283)(0.27)\left(\frac{0.50}{0.402}-1\right)}{26\left(\frac{0.50}{0.402}+1\right)}}$$

$$F = \frac{9.216\left[1 + \frac{(2.665)(0.74)}{(0.87)(1.341)}\right]}{610 - 94.7}$$

$$= 0.0481$$

$$h_i = F\, G_i^{0.8}\, C_p \left(\frac{\mu_i}{D_i}\right)^{0.2}$$

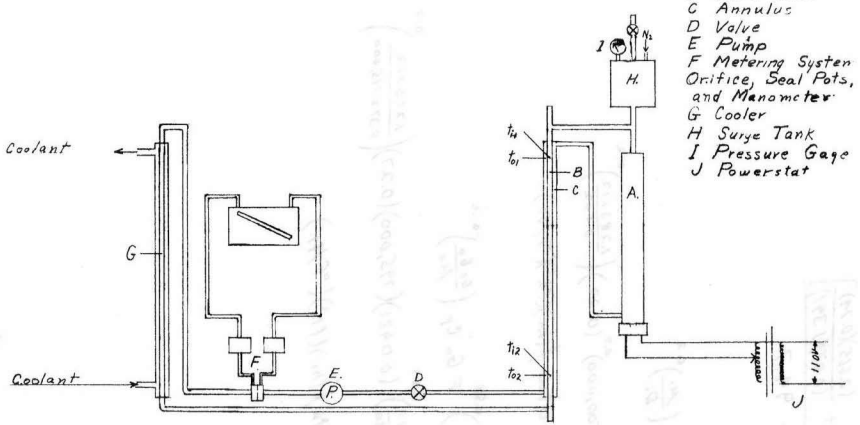
$$= 0.0481(2{,}500{,}000)^{0.8}(0.27)\left(\frac{1.283 \times 12}{0.402}\right)^{0.2}$$

$$= 3538 \quad Btu./(hr.)(ft.^2)(°F/ft.)$$

$$h_o = 0.87\left(\frac{D_e}{D_o}\right)^{0.53} F\, G_o\, C_p \left(\frac{D_e G_o}{\mu_o}\right)^{-0.2}$$

$$= 0.87\left(\frac{0.87}{0.50}\right)^{0.53}(0.0481)(795{,}000)(0.27)\left(\frac{1.283 \times 12}{0.37 \times 795{,}000}\right)^{0.2}$$

$$= 1686 \quad Btu./(hr.)(ft.^2)(°F/ft.)$$



MINE SAFETY APPLIANCES CO.
CALLERY, PA.

HEAT EXCHANGER NO. 1
DRAWN BY, R.T. - 10-2-46
DRAWING NO. C-154-4

Plate 1